

# Production of aviation and marine fuels by biomass liquefaction and upgrading by HDO

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**VTT**



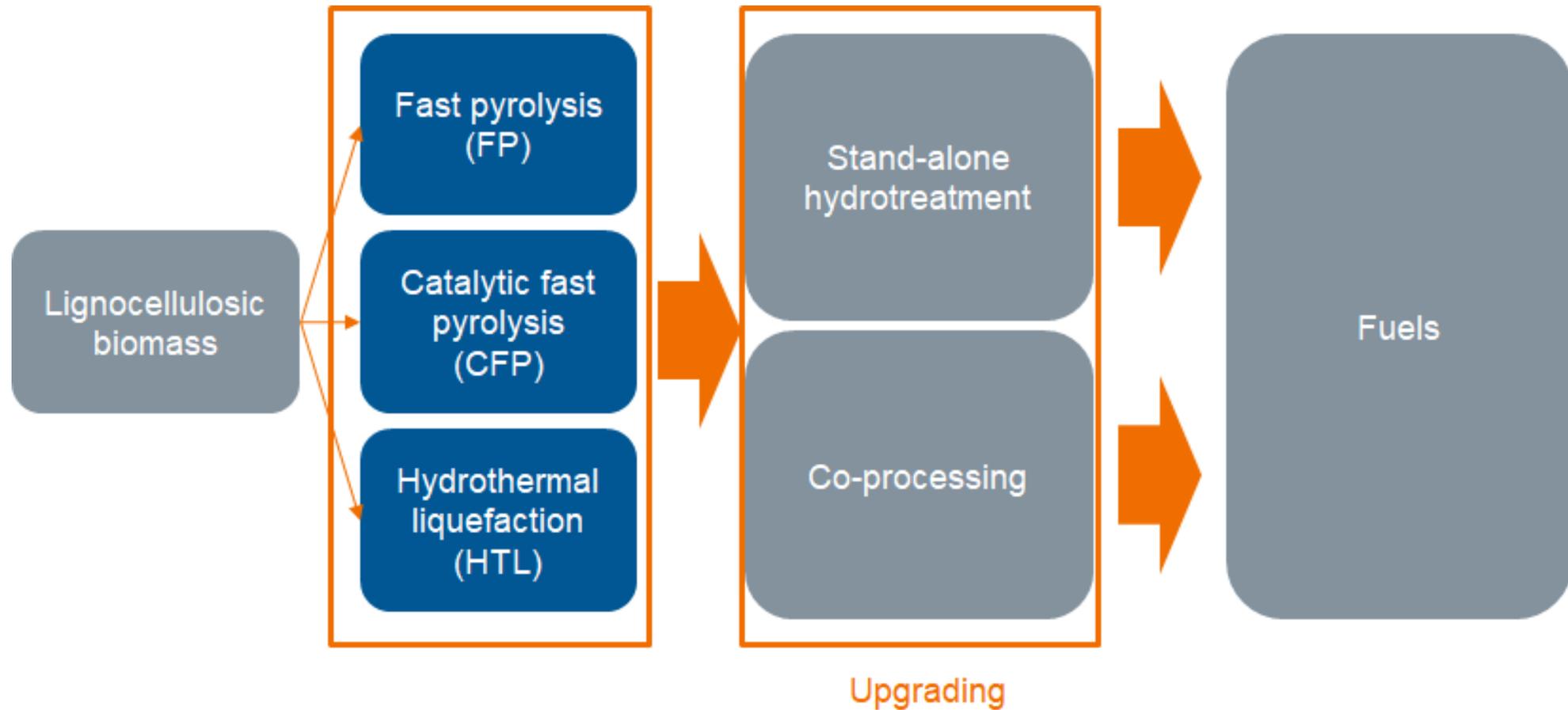
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# Outline

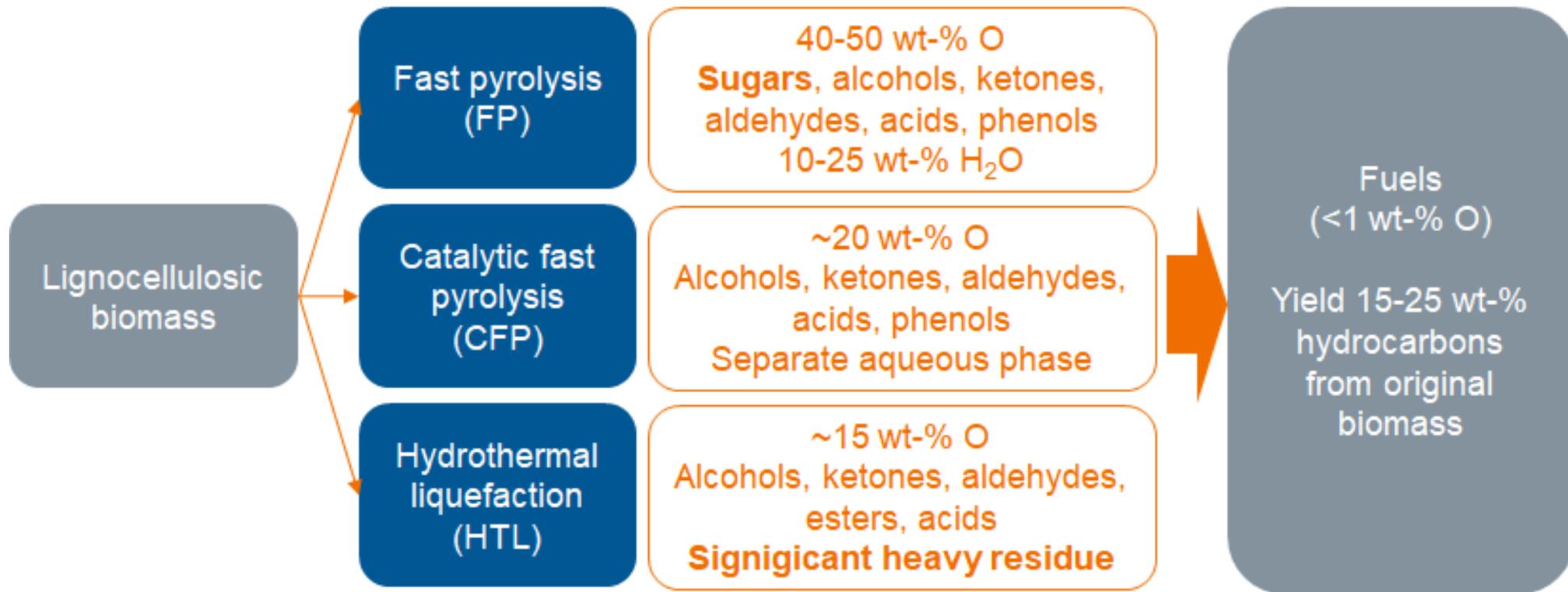
1. Introduction to biomass liquefaction and upgrading by hydrotreatment
2. Catalytic slurry hydrotreatment
3. Hydrothermal HDO
4. Summary



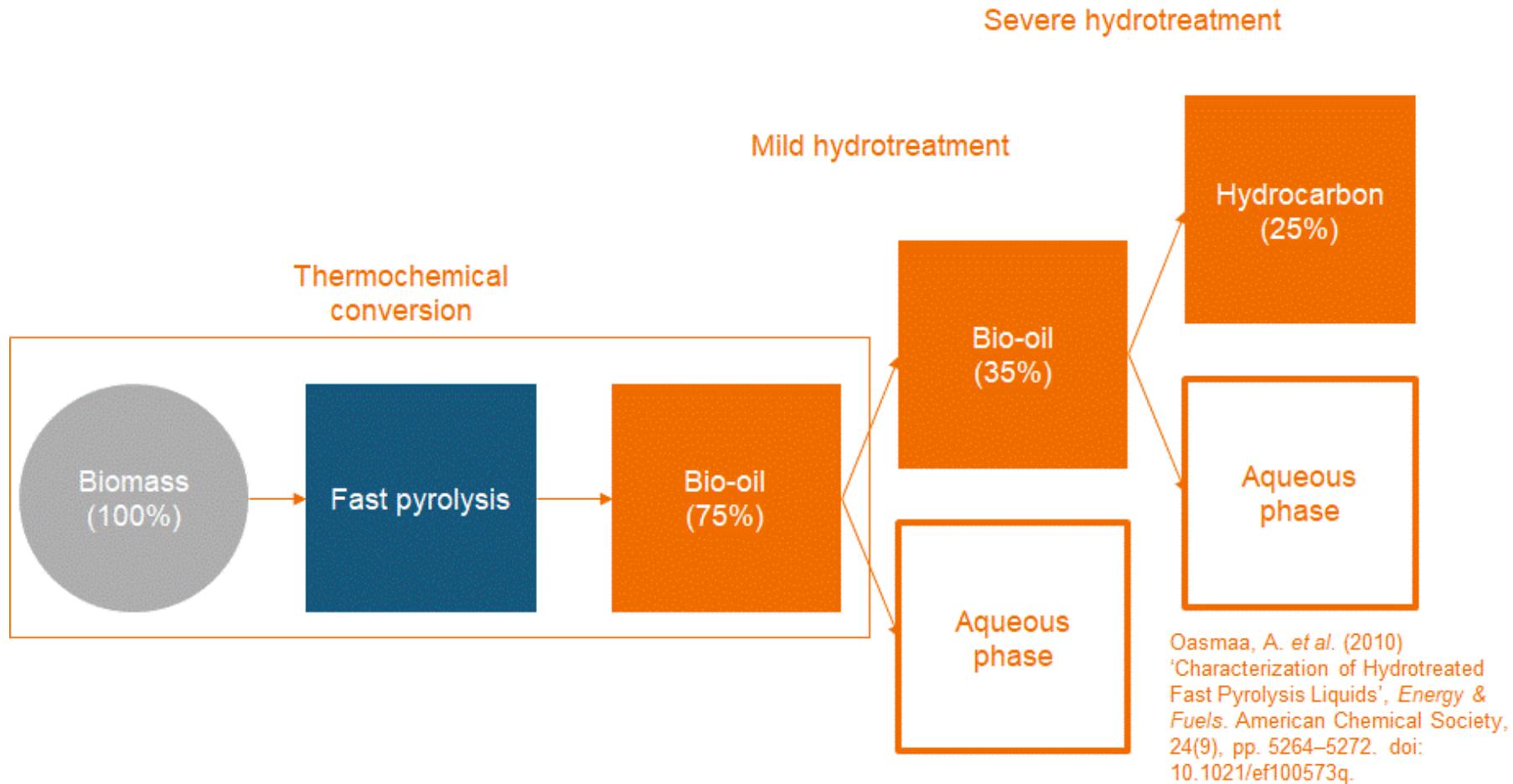
# Biofuels from lignocellulosic biomass by liquefaction



# Biofuels from lignocellulosic biomass by liquefaction



# Bio-oils liquefaction by fast pyrolysis and upgrading by HDO



# Instability of bio-oils

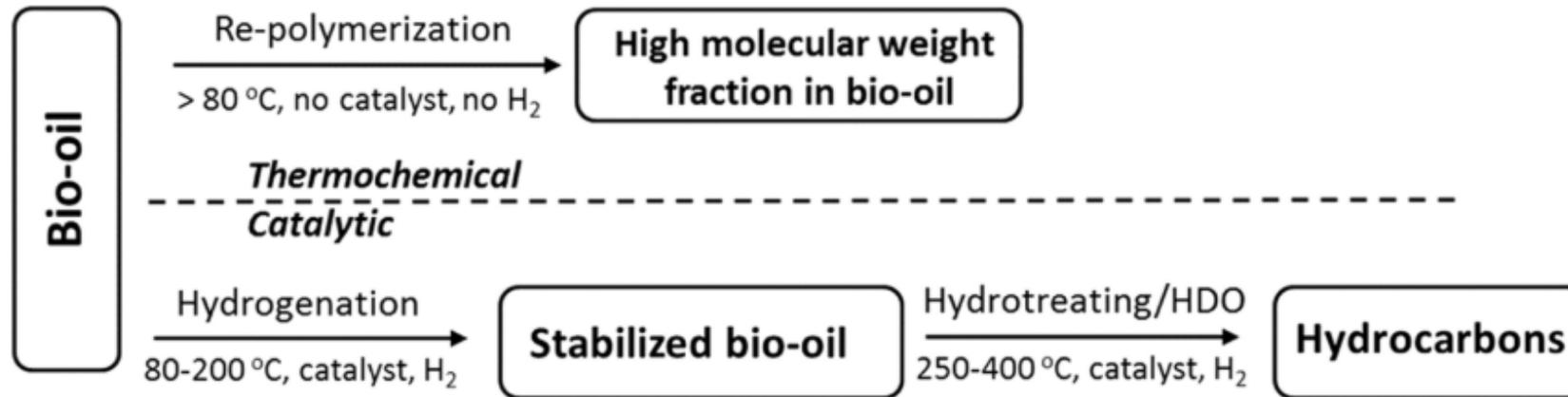


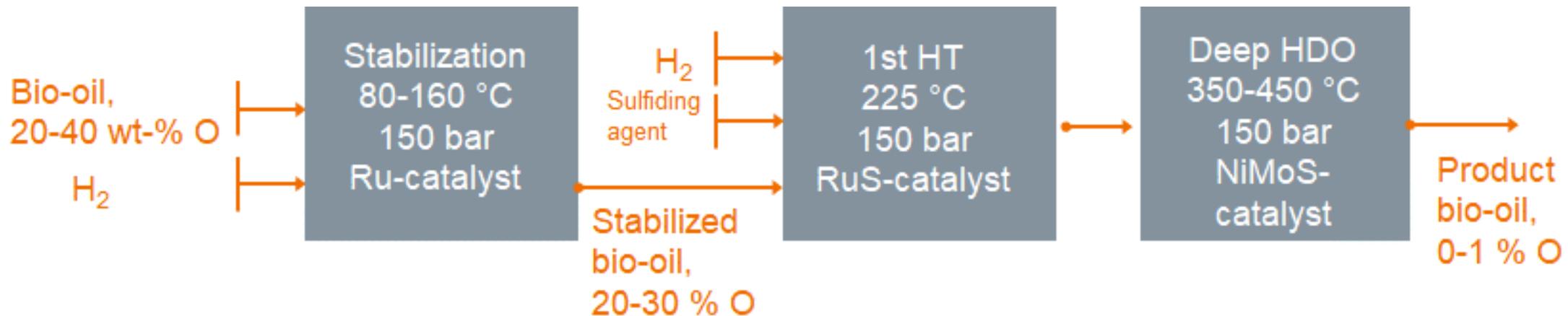
Figure from Wang *et al.* 2016

- Bio-oils tends to thermally repolymerize and form plugs in process units
- First signs of thermal condensation at < 100 °C, severe at high temperature
- High carbohydrate and carbonyl content



# Stepwise processing

- The plug formation can be hindered by hydroprocessing the bio-oil in multiple steps in fixed bed hydrotreater reactors
- Problems: expensive catalysts, deactivation during 1st stabilising hydrogenation step due to sulphur and coke formation



# VTT activities in bio-oils upgrading by HDO

- BL2F – Black liquor to fuel
  - Integrated HTL and upgrading of black liquor to fuels
  - Performing the HDO in near-critical or supercritical water
- BioFlex
  - Low cost methods to produce marine fuels by fast pyrolysis and upgrading by fixed bed HDO
- Catalytic Slurry Hydrotreatment
  - Catalyst development, regeneration and recovery for slurry-phase hydrotreatment of bio-oil



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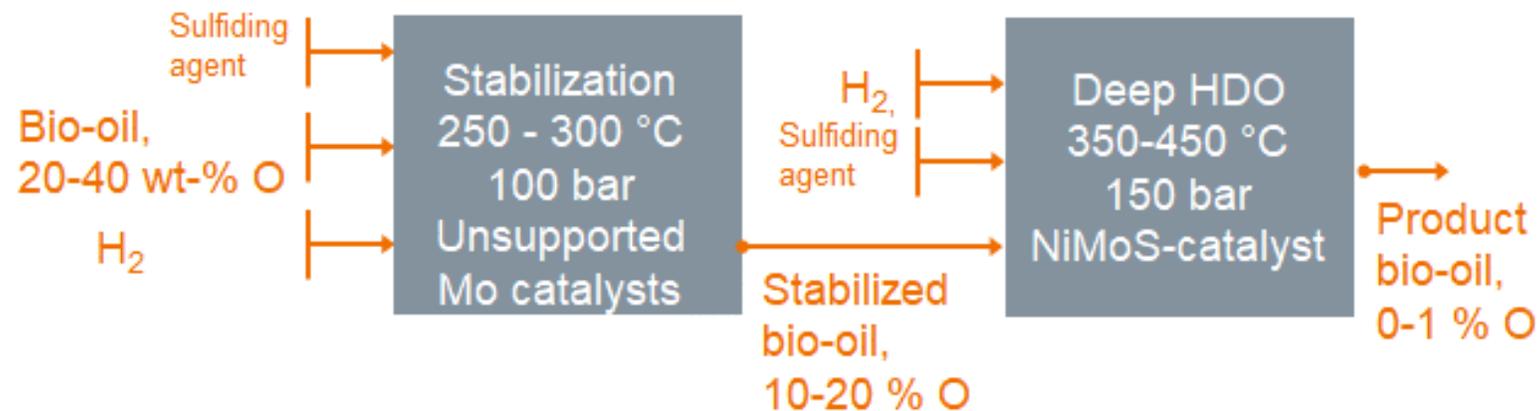
# Catalytic slurry hydrotreatment



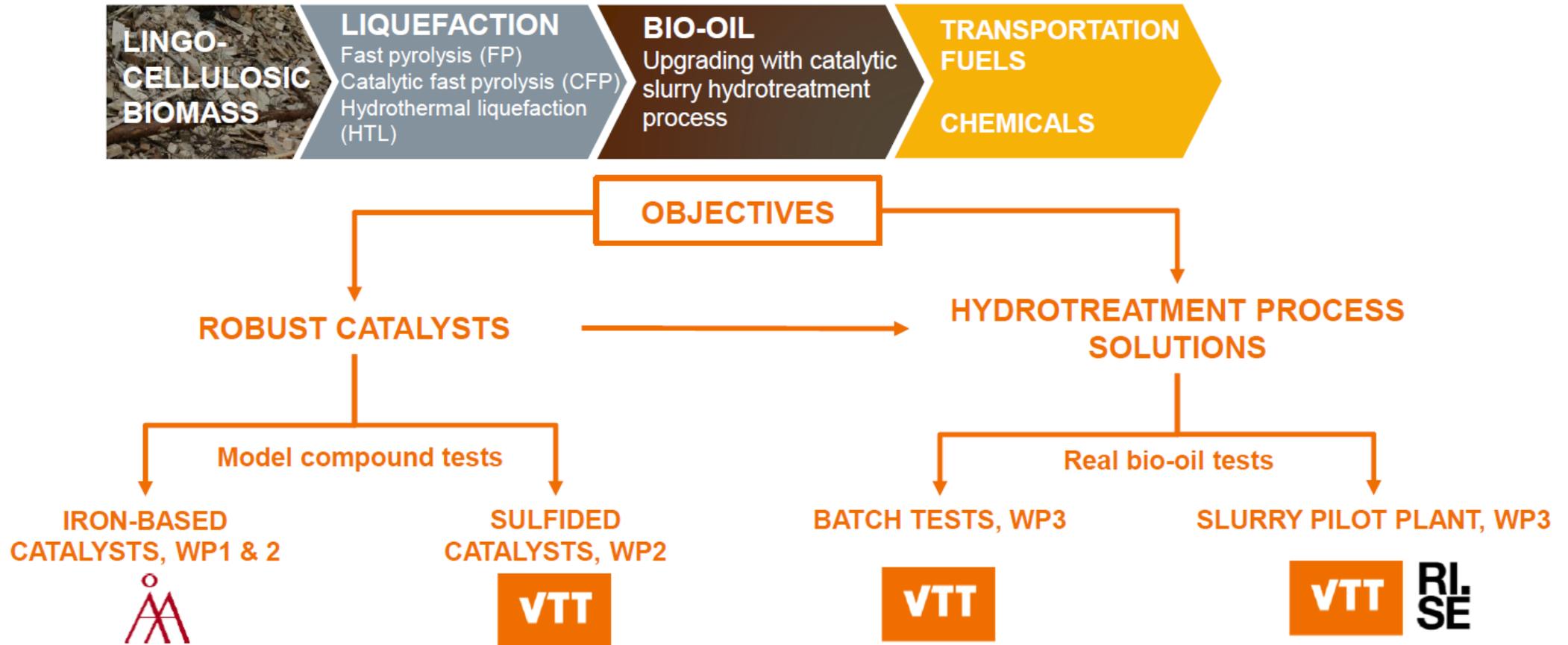
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# Alternative: slurry hydrotreatment applied for the stabilisation

- State-of-the-art: multi-staged approach
  - Bio-oil stabilization by slurry hydrotreatment applying sulfided Mo-based catalysts
    - Continuous addition of fresh and removal of spent catalyst enabled
  - Rest oxygen removal by fixed bed hydrotreatment by supported sulfided catalysts
    - Severity defined by product specification

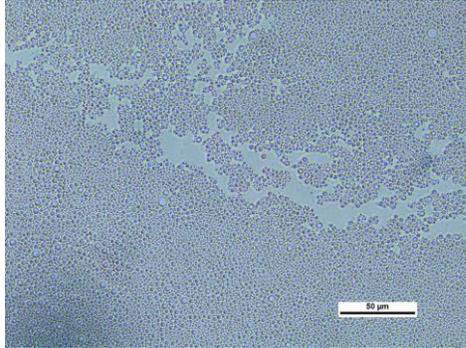


# CaSH - Catalytic slurry hydrotreatment



# Preparation of unsupported Mo and promoted Mo catalysts

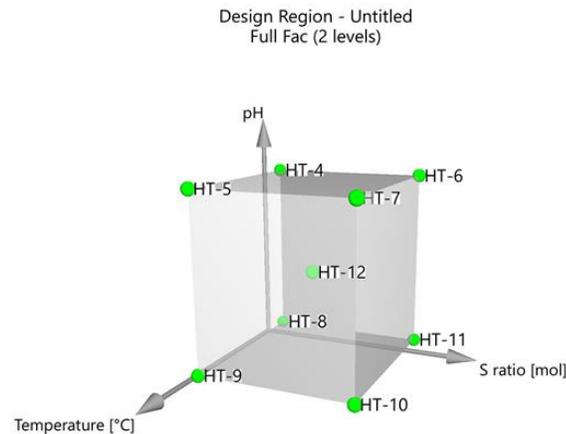
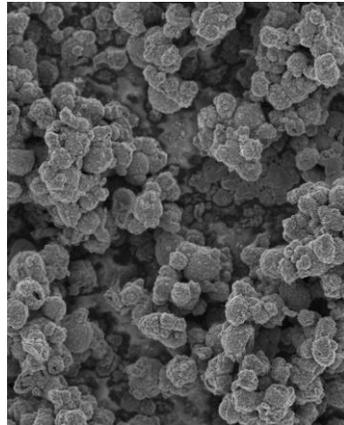
Emulsion- templated synthesis



HDO activity correlation with:

- Emulsion properties
- Precursor properties
- Emulsion sulfidation

One-pot hydrothermal precipitation

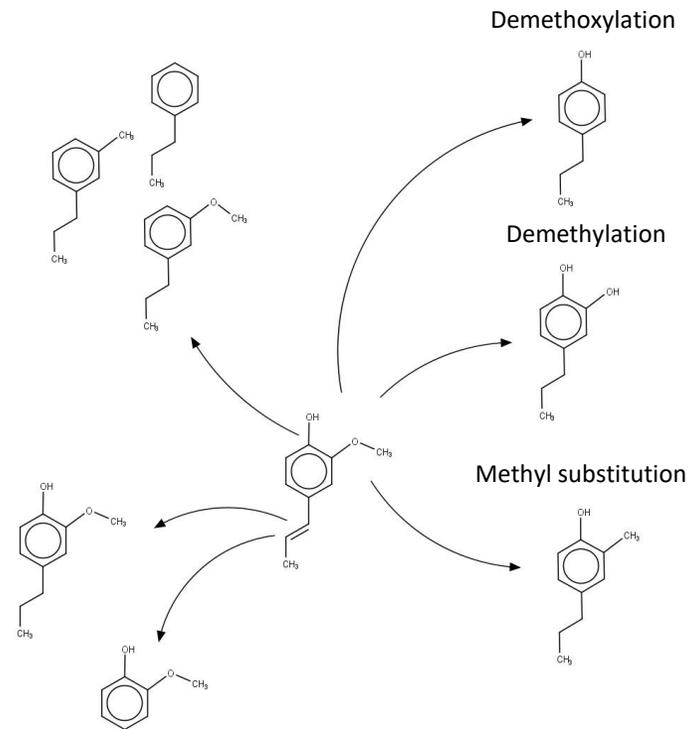
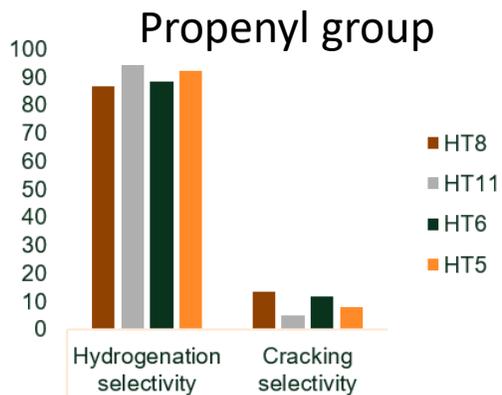
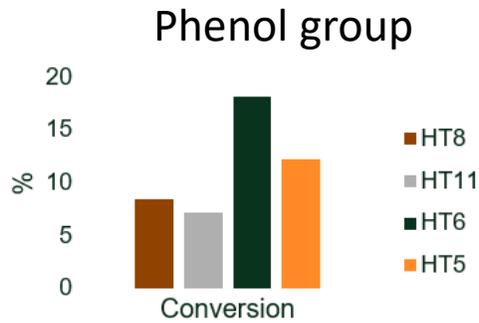


Catalyst properties and HDO activity correlation with:

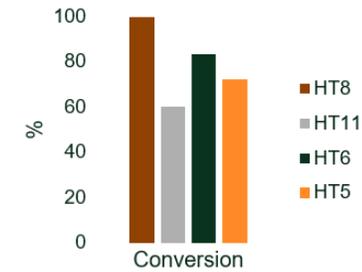
- Synthesis pH
- Synthesis temperature
- Sulfur amount in synthesis



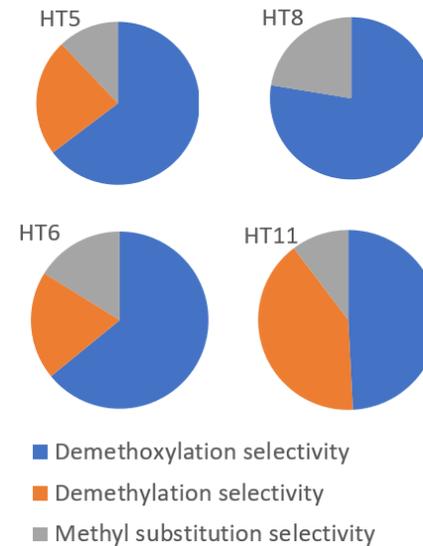
# Catalyst preparation affecting HDO activity



## Methoxy group



## Selectivity



# Tests with real bio-oils

## BATCH TEST RUNS

VTT

- ✓ Batch reactor operation validated with model compounds
- Transition to real bio-oil starting in early 2022

## ACTIVITIES

- Identifying and procuring suitable bio-oils
- Discharged catalyst characterization
- Production of larger catalyst batch for slurry pilot test run

## SLURRY PILOT PLANT

VTT

RISE

- Test run performed with the best catalyst from WP1 and WP2 catalyst development.
- Objective few test runs, in the range of total 50 hours of operation.

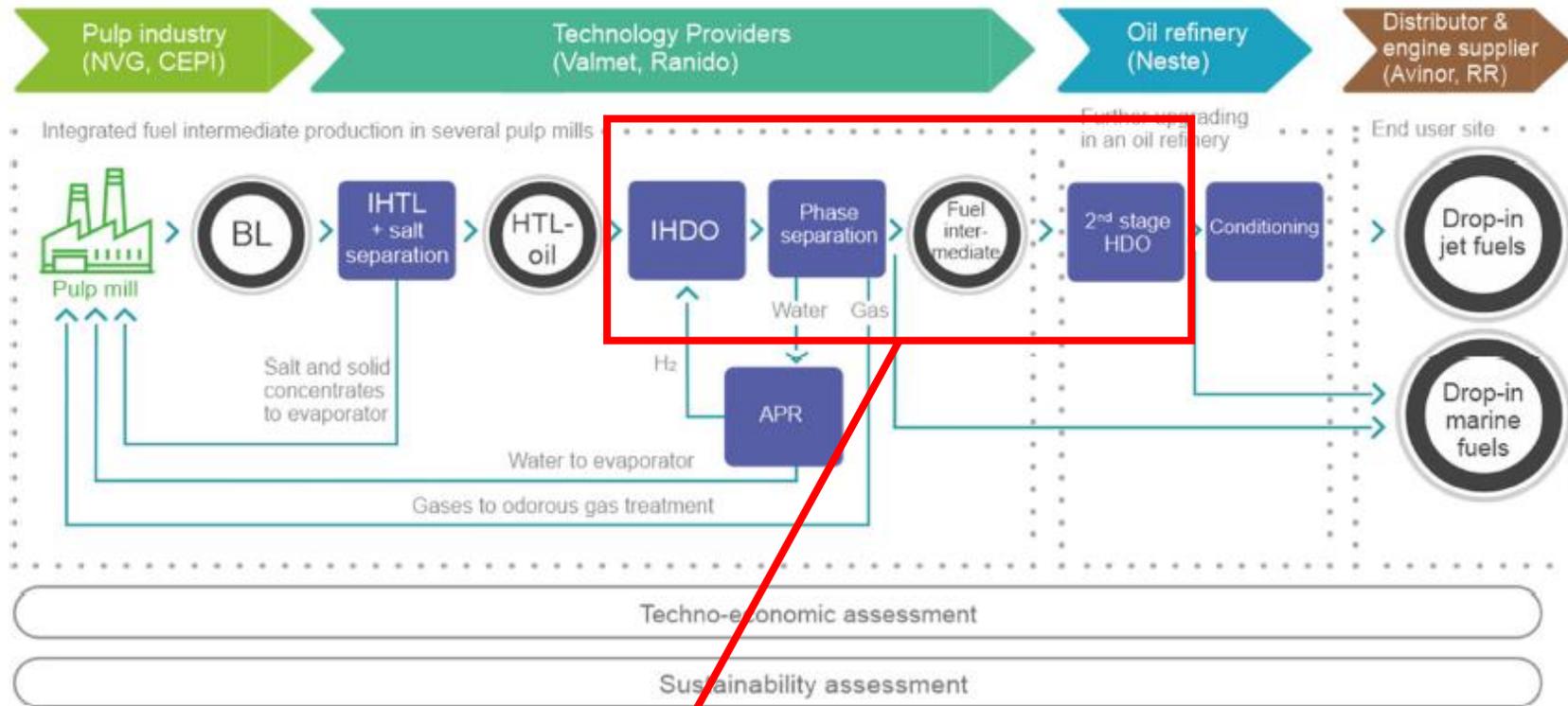


# Hydrothermal HDO



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# Another alternative: BL2F upgrading concept



IHDO = HDO in hydrothermal conditions



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# Hydrothermal HDO

HDO in hydrothermal conditions in BL2F

- Utilization of biocrude from HTL in aqueous environment
- Performing hydrothermal catalytic HDO in near critical or supercritical conditions

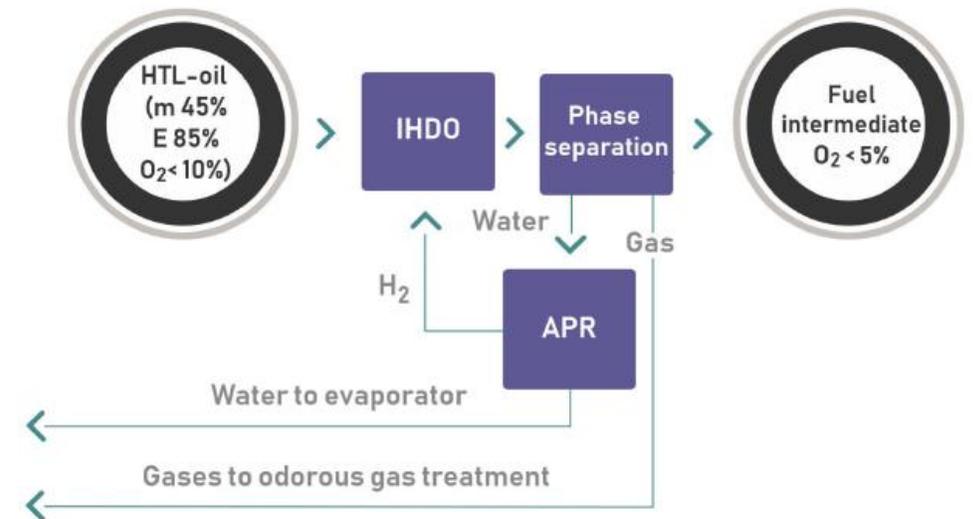
Benefits:

- No need to separate water before IHDO
- Water can act as solvent of hydrocarbons in such conditions
- Hydrogen can be generated in situ by catalytic transfer hydrogenation and APR in such conditions
- Reaction conditions can protect catalyst from deactivation by coke

Challenges:

- Residues of salts from IHTL to IHDO affect the catalyst deactivation
- Catalyst materials should tolerate aqueous near/supercritical conditions

## Integrated HydroDeOxygenation (IHDO)

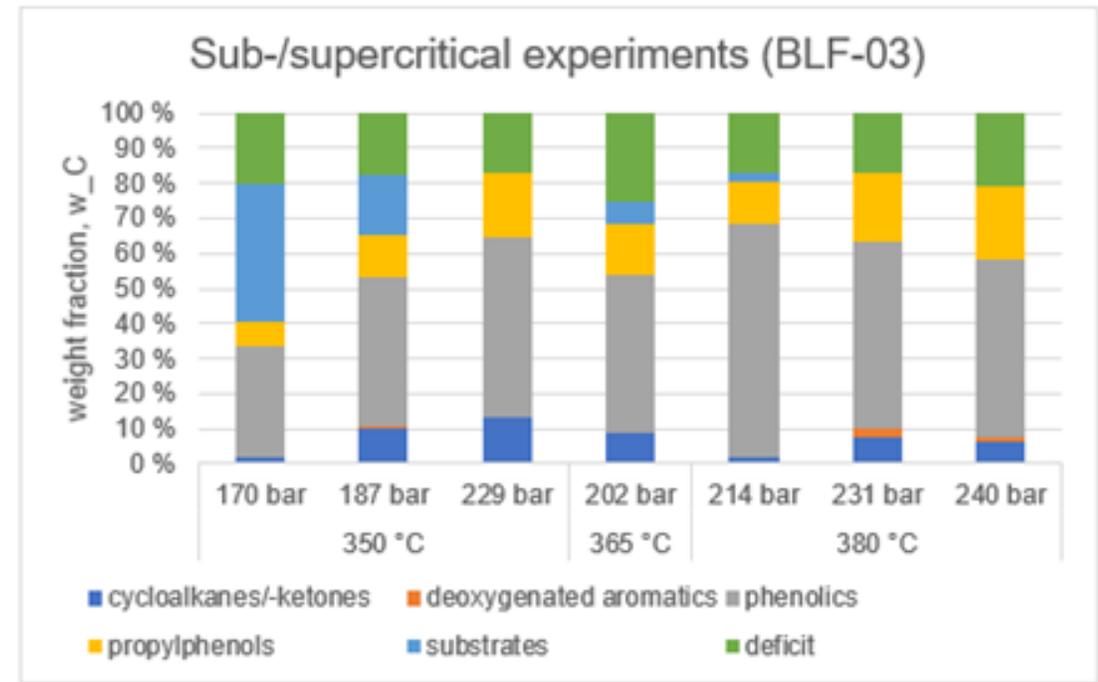
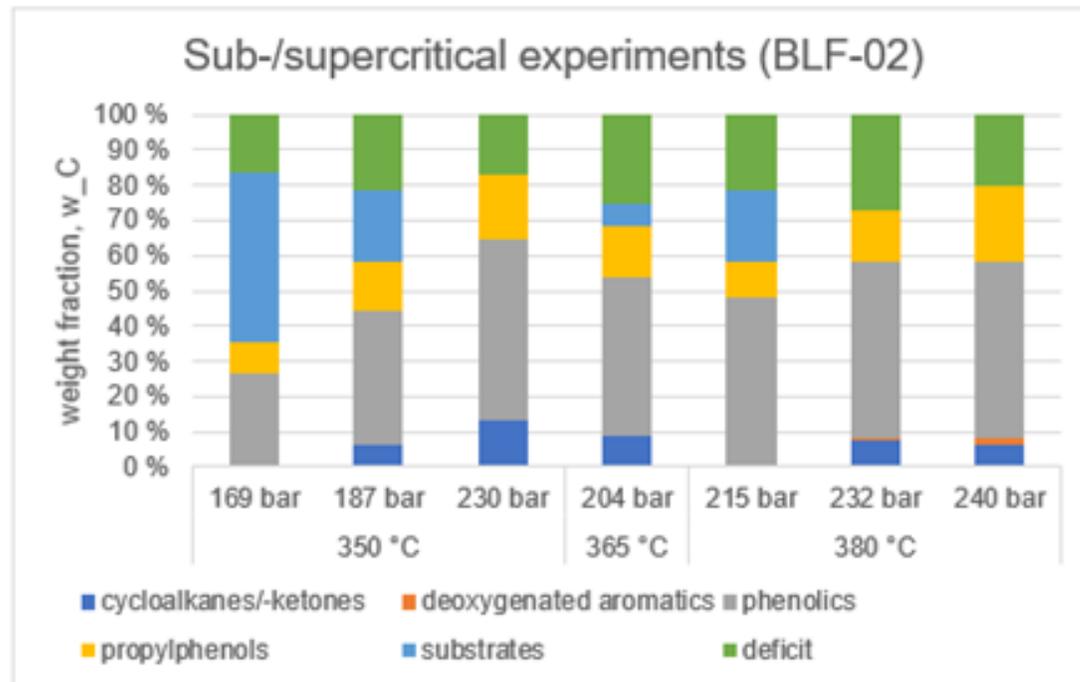


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*Green Chem.*, **23**, 2021, 1114; *Catalysis Communications*, **90**, 2017, 47-50; *Chemical Engineering Journal*, **407**, 2021, 126332.

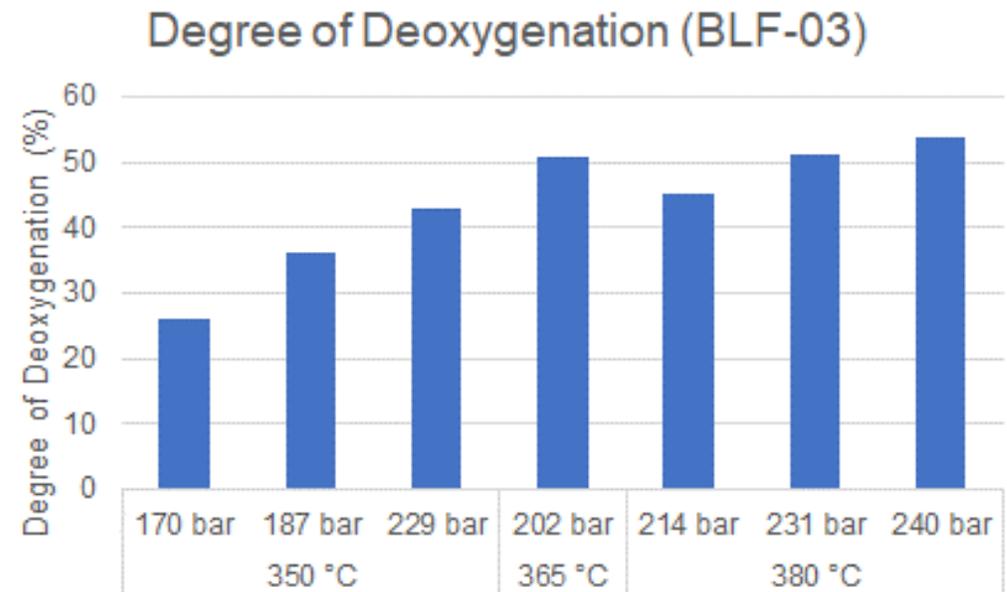
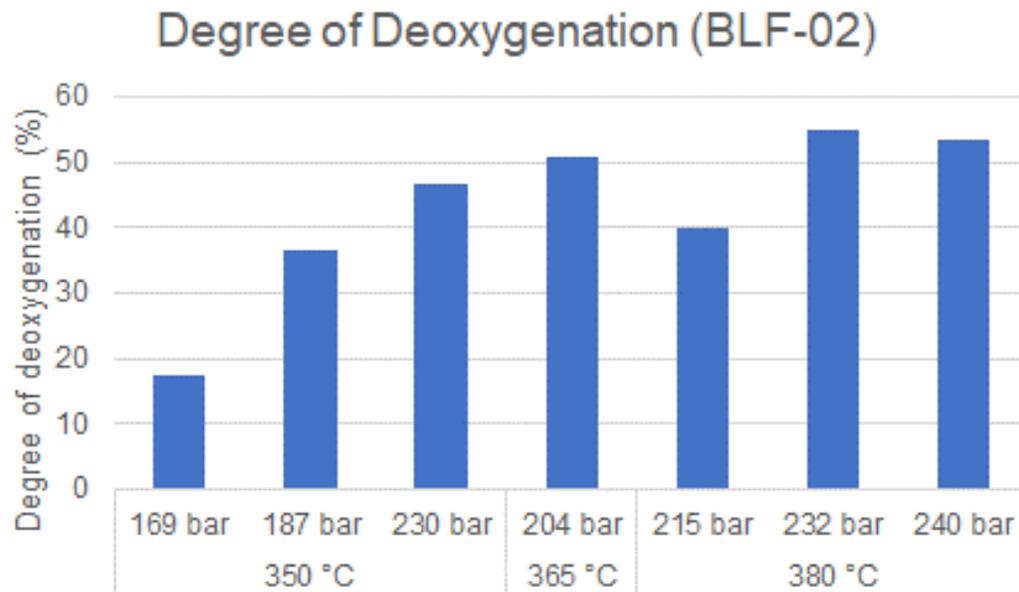
# Hydrothermal HDO – model component testing

- HDO experiments of isoeugenol and 4-methylcatechol
  - 2 h reaction time, 2 g model compounds, 1g catalyst, 150 ml H<sub>2</sub>O



# Hydrothermal HDO – model component testing

- BLF-03 performs slightly better especially in the “milder” conditions



# Summary

- Upgrading of bio-oils to transportation fuels challenging due to instability of bio-oils and impurities in bio-oils (sulfur etc.)
- New solutions needed to commercialize bio-oils upgrading by HDO
  - Slurry hydroprocessing (CaSH project)
  - Hydrothermal HDO (BL2F project)
- Catalysts have been developed and tested for these two upgrading technologies
  - So far mainly tests with model components
- Next steps: tests with real bio-oil feeds



# Thank you!

## Get in touch with the project:

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