

Production of aviation and marine fuels by biomass liquefaction and upgrading by HDO

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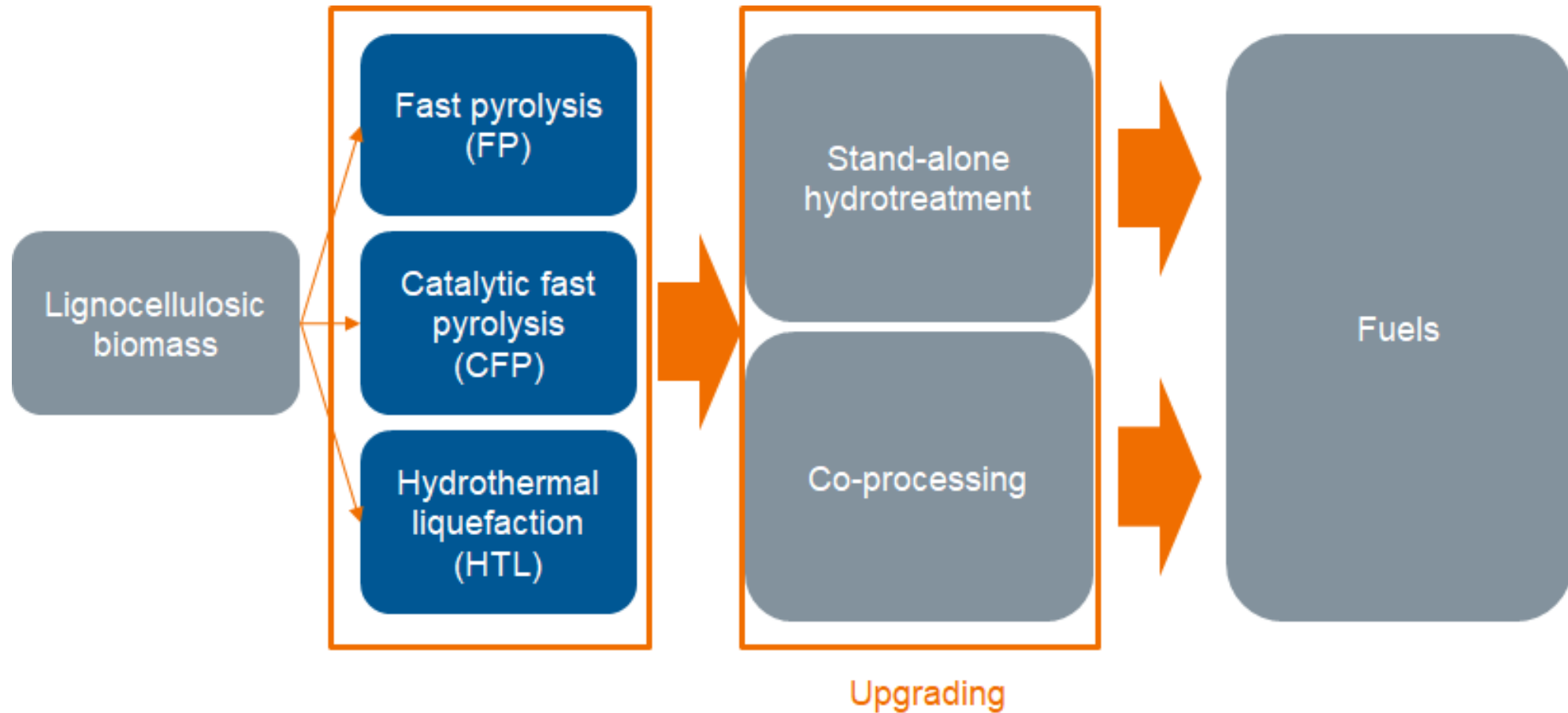
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Outline

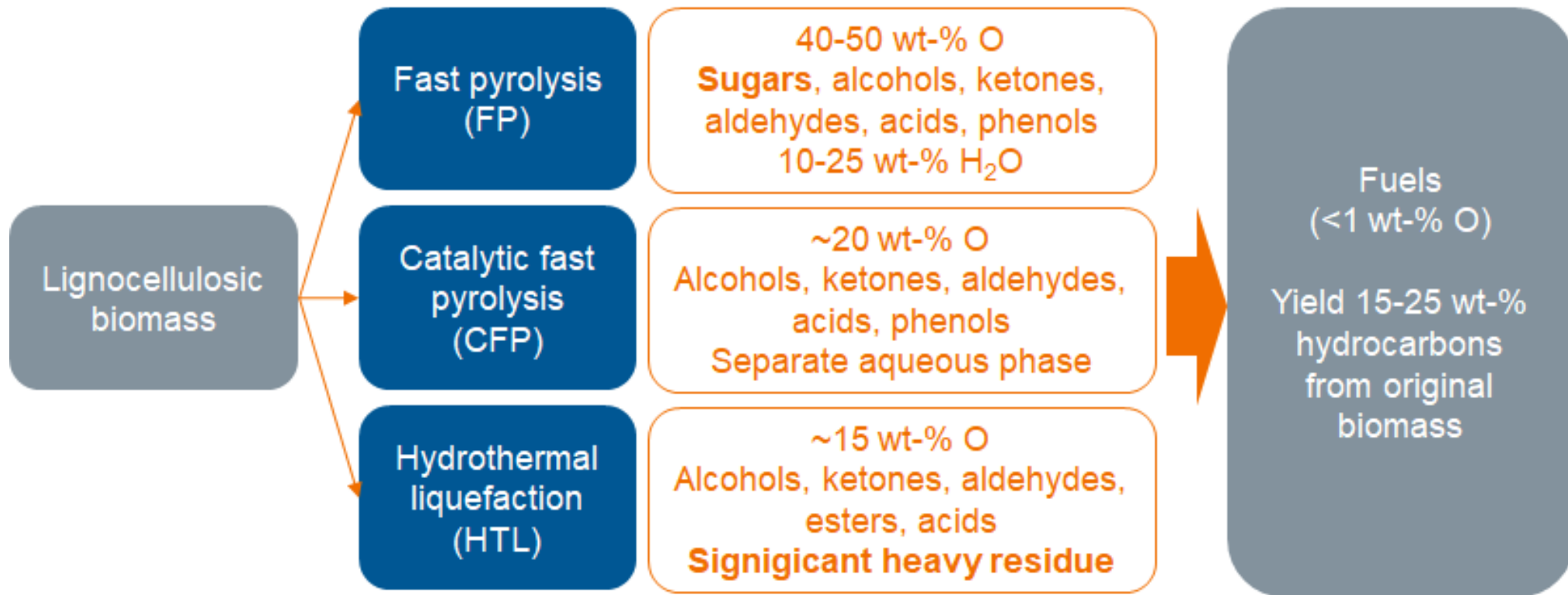
1. Introduction to biomass liquefaction and upgrading by hydrotreatment
2. Catalytic slurry hydrotreatment
3. Hydrothermal HDO
4. Summary



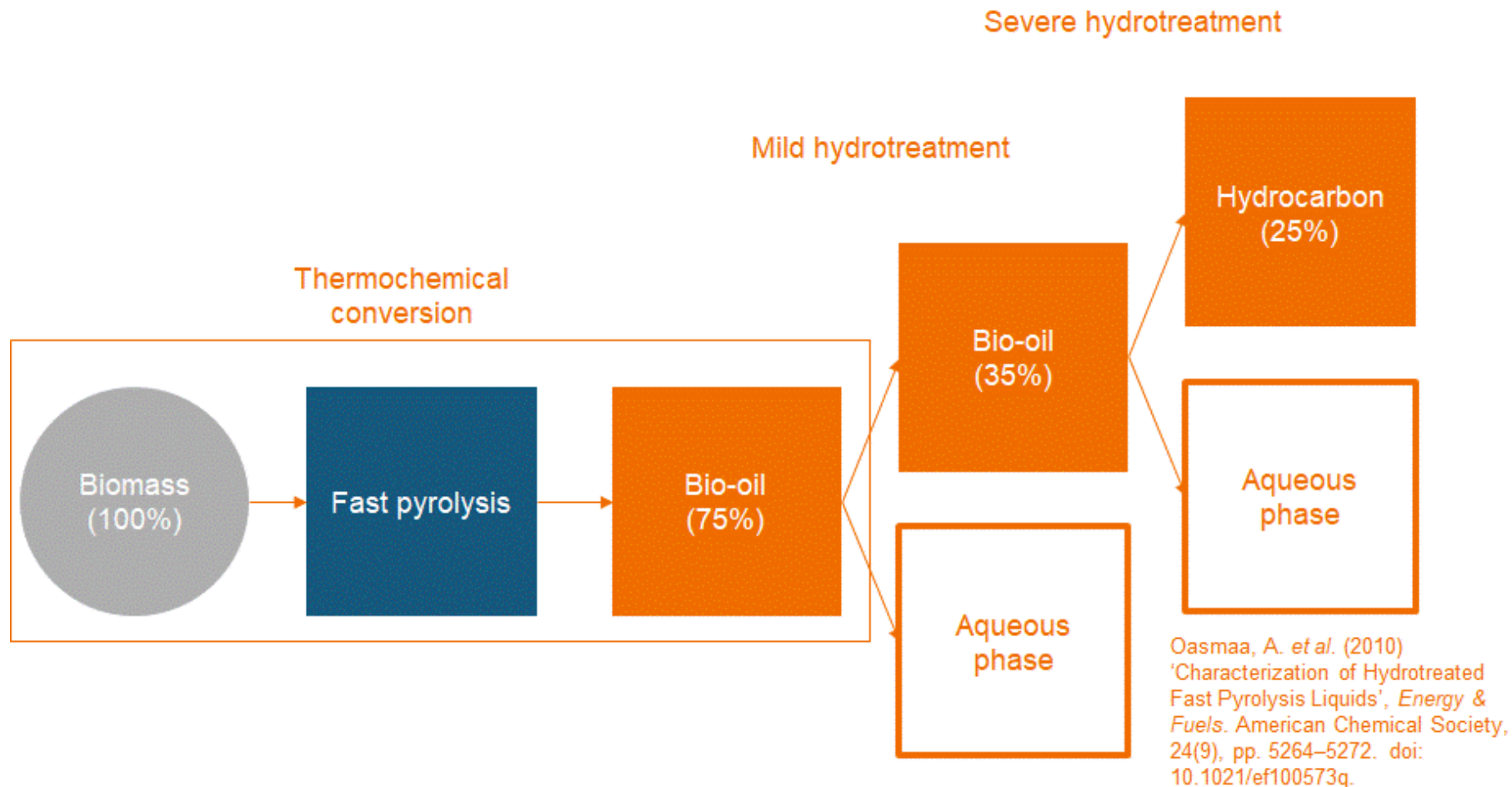
Biofuels from lignocellulosic biomass by liquefaction



Biofuels from lignocellulosic biomass by liquefaction



Bio-oils liquefaction by fast pyrolysis and upgrading by HDO



Instability of bio-oils

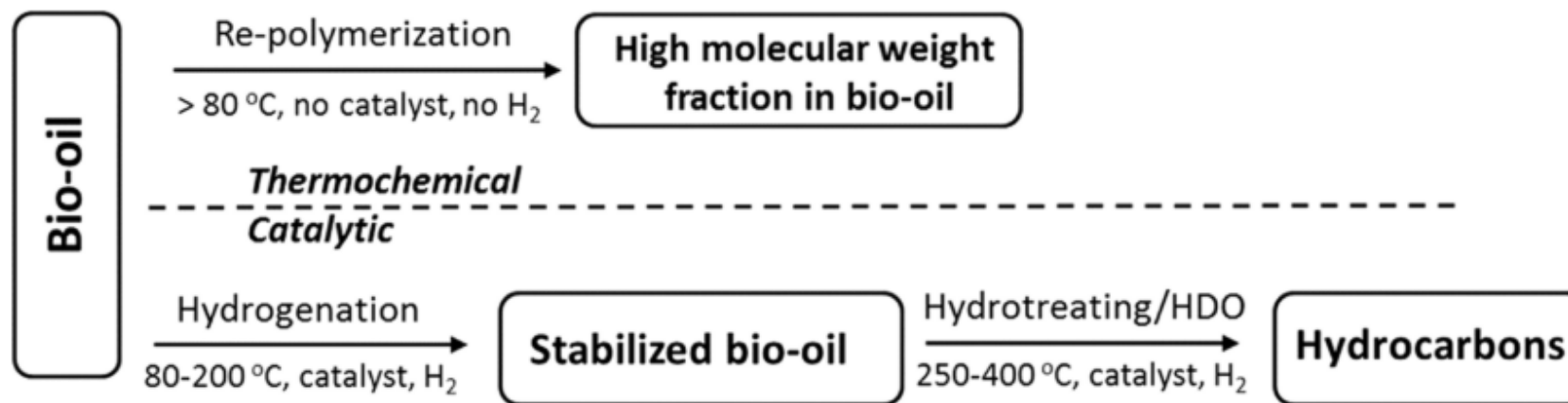


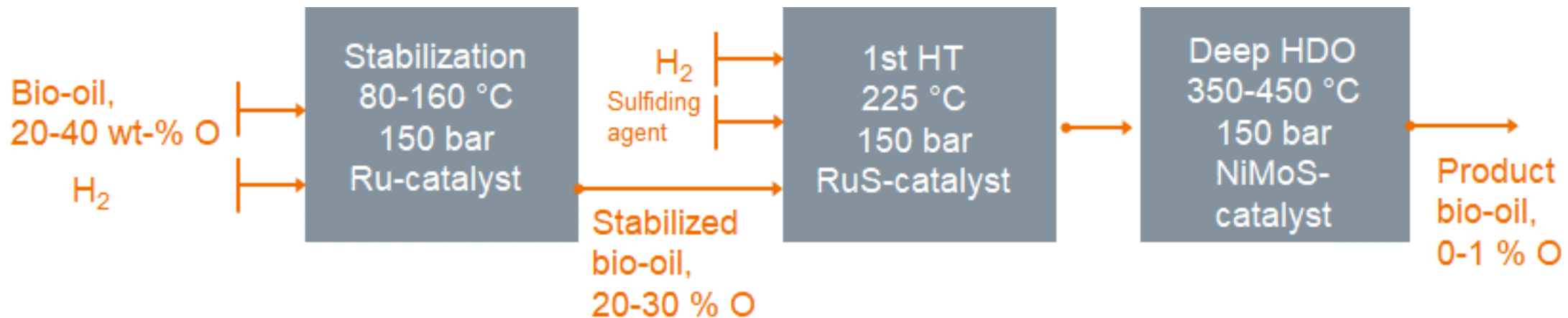
Figure from Wang *et al.* 2016

- Bio-oils tends to thermally repolymerize and form plugs in process units
- First signs of thermal condensation at <100 °C, severe at high temperature
- High carbohydrate and carbonyl content



Stepwise processing

- The plug formation can be hindered by hydroprocessing the bio-oil in multiple steps in fixed bed hydrotreater reactors
- Problems: expensive catalysts, deactivation during 1st stabilising hydrogenation step due to sulphur and coke formation



VTT activities in bio-oils upgrading by HDO

- BL2F – Black liquor to fuel
 - Integrated HTL and upgrading of black liquor to fuels
 - Performing the HDO in near-critical or supercritical water
- BioFlex
 - Low cost methods to produce marine fuels by fast pyrolysis and upgrading by fixed bed HDO
- Catalytic Slurry Hydrotreatment
 - Catalyst development, regeneration and recovery for slurry-phase hydrotreatment of bio-oil



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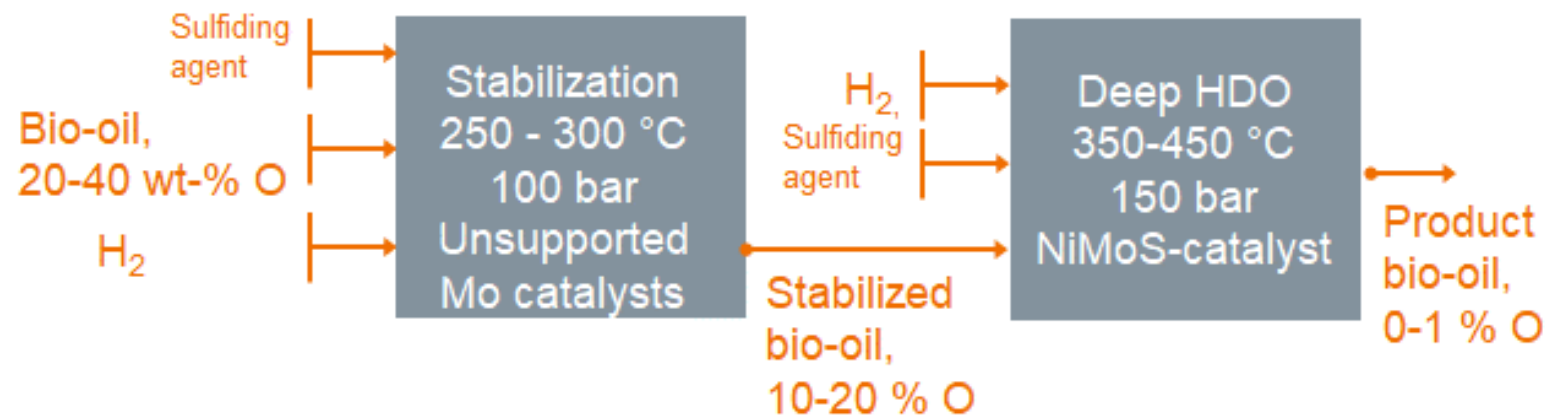
Catalytic slurry hydrotreatment



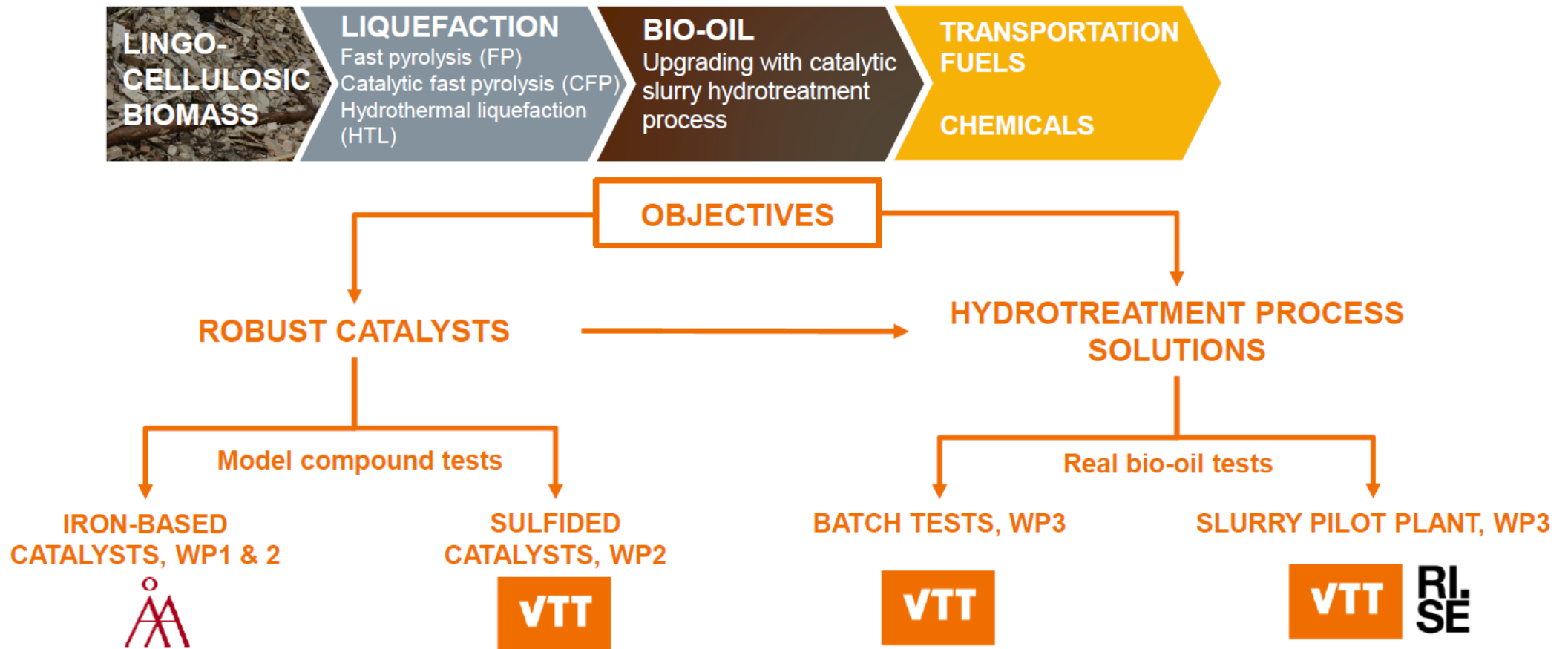
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Alternative: slurry hydrotreatment applied for the stabilisation

- State-of-the-art: multi-staged approach
 - Bio-oil stabilization by slurry hydrotreatment applying sulfided Mo-based catalysts
 - Continuous addition of fresh and removal of spent catalyst enabled
 - Rest oxygen removal by fixed bed hydrotreatment by supported sulfided catalysts
 - Severity defined by product specification

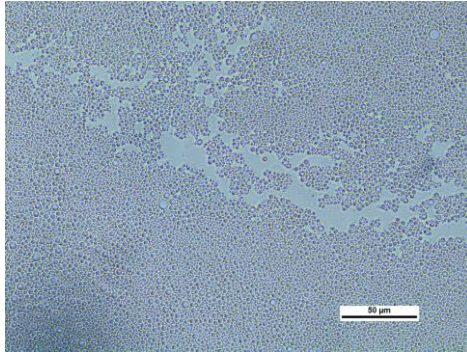


CaSH - Catalytic slurry hydrotreatment



Preparation of unsupported Mo and promoted Mo catalysts

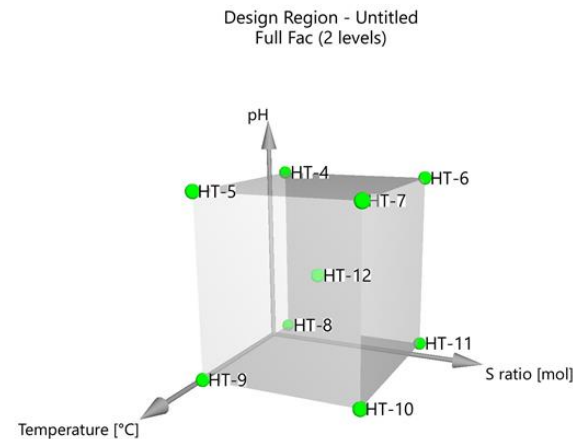
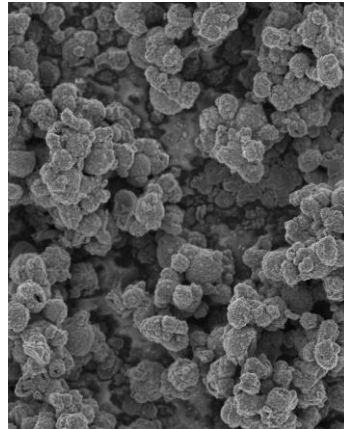
Emulsion- templated synthesis



HDO activity correlation with:

- Emulsion properties
- Precursor properties
- Emulsion sulfidation

One-pot hydrothermal precipitation



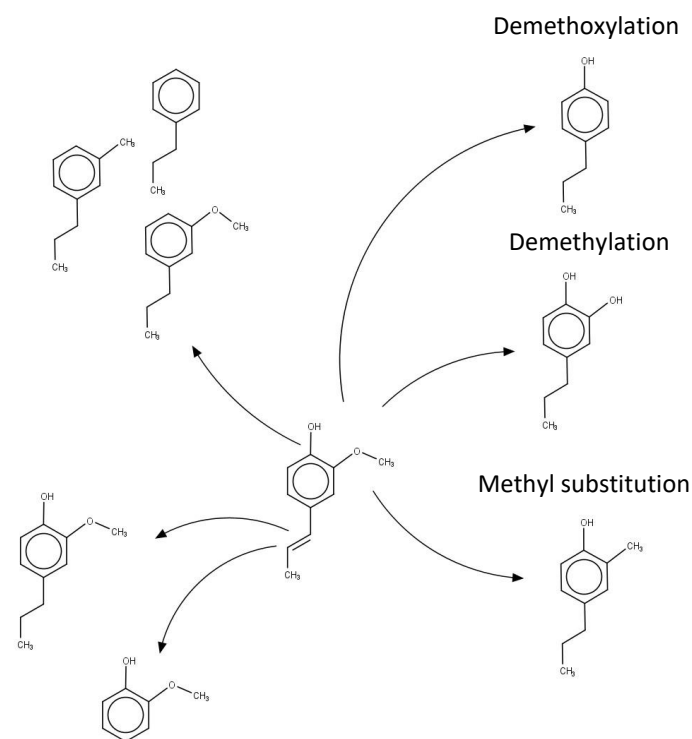
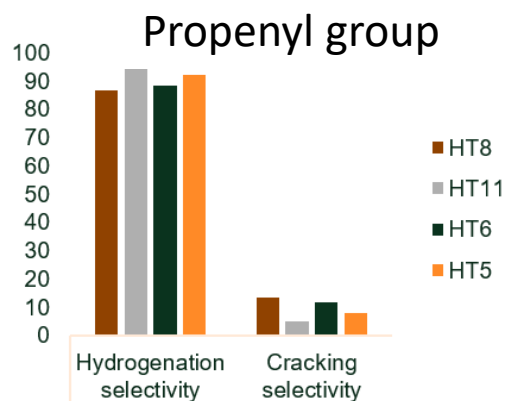
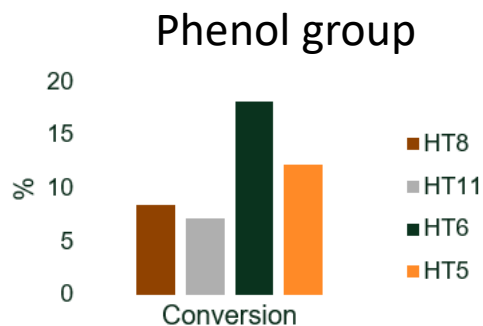
Catalyst properties and HDO activity correlation with:

- Synthesis pH
- Synthesis temperature
- Sulfur amount in synthesis

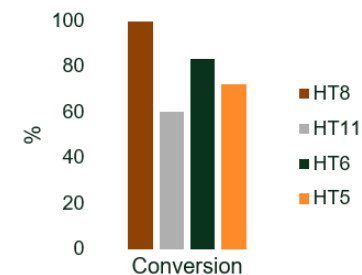


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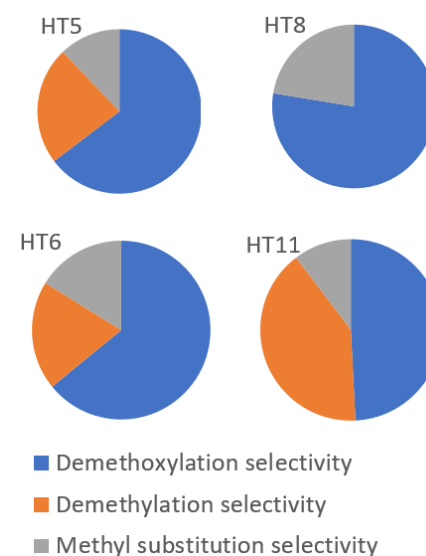
Catalyst preparation affecting HDO activity



Methoxy group



Selectivity



Tests with real bio-oils

BATCH TEST RUNS

VTT

- ✓ Batch reactor operation validated with model compounds
- Transition to real bio-oil starting in early 2022

ACTIVITIES

- Identifying and procuring suitable bio-oils
- Discharged catalyst characterization
- Production of larger catalyst batch for slurry pilot test run

SLURRY PILOT PLANT

VTT

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- Test run performed with the best catalyst from WP1 and WP2 catalyst development.
- Objective few test runs, in the range of total 50 hours of operation.

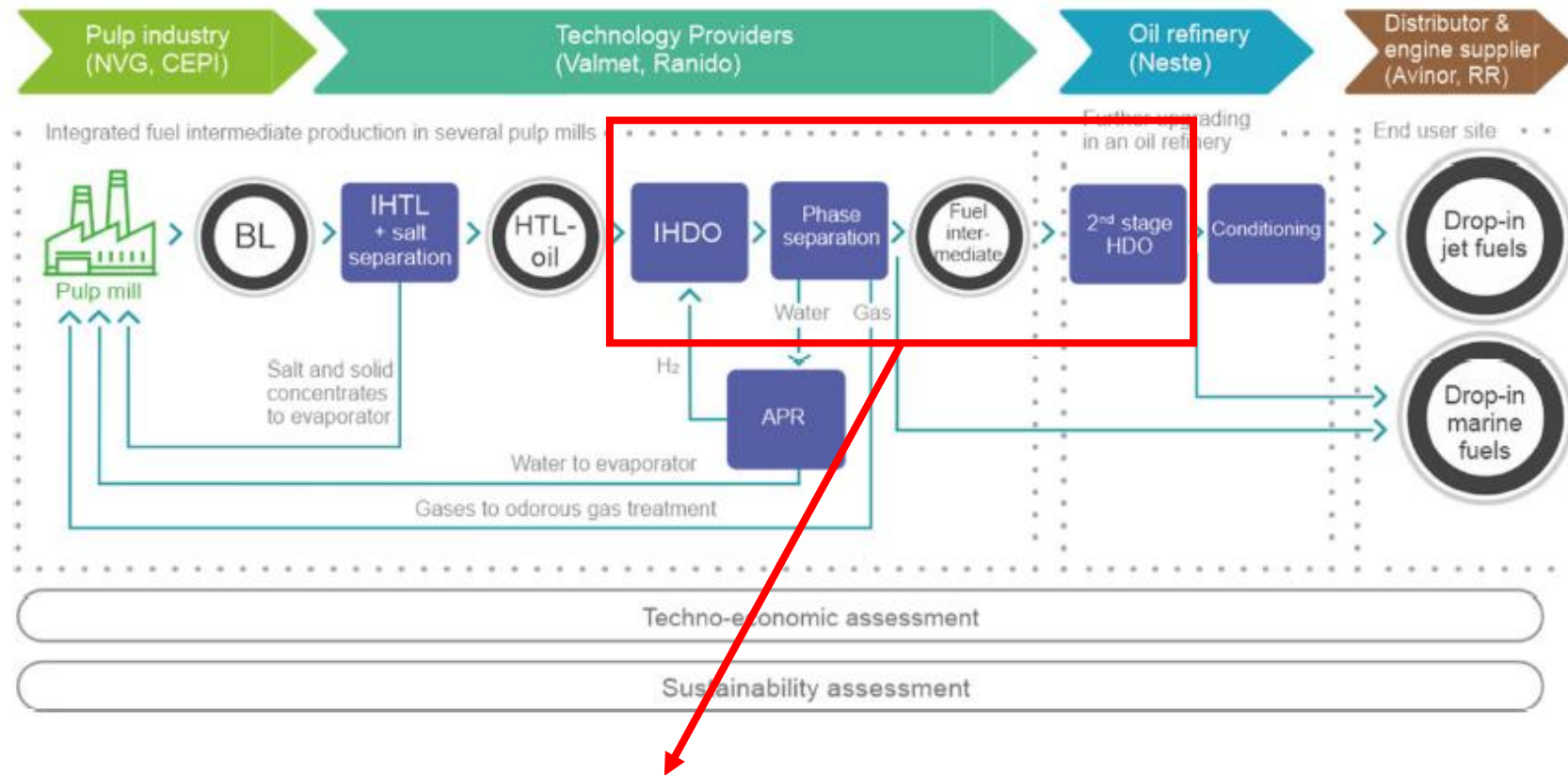


Hydrothermal HDO



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Another alternative: BL2F upgrading concept



IHDO = HDO in hydrothermal conditions



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Hydrothermal HDO

HDO in hydrothermal conditions in BL2F

- Utilization of biocrude from HTL in aqueous environment
- Performing hydrothermal catalytic HDO in near critical or supercritical conditions

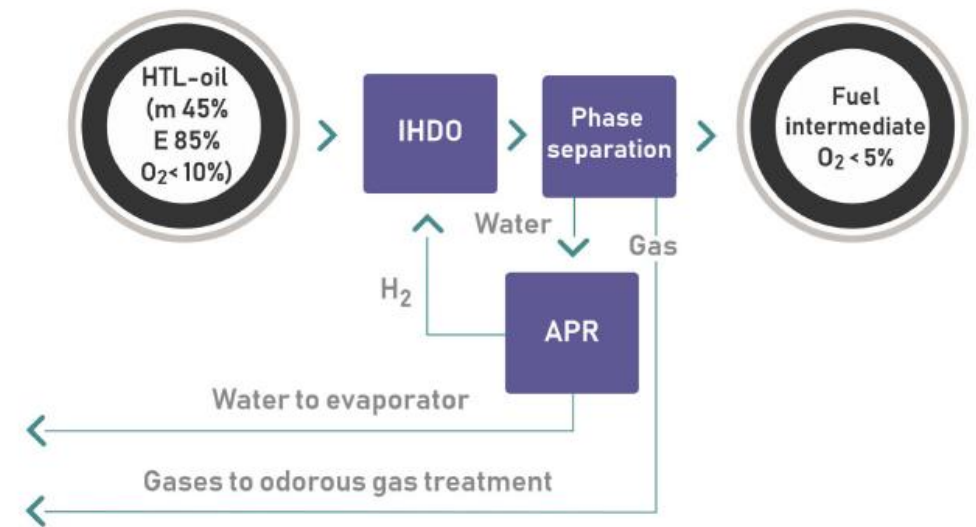
Benefits:

- No need to separate water before IHDO
- Water can act as solvent of hydrocarbons in such conditions
- Hydrogen can be generated in situ by catalytic transfer hydrogenation and APR in such conditions
- Reaction conditions can protect catalyst from deactivation by coke

Challenges:

- Residues of salts from IHTL to IHDO affect the catalyst deactivation
- Catalyst materials should tolerate aqueous near/supercritical conditions

Integrated HydroDeOxygenation (IHDO)



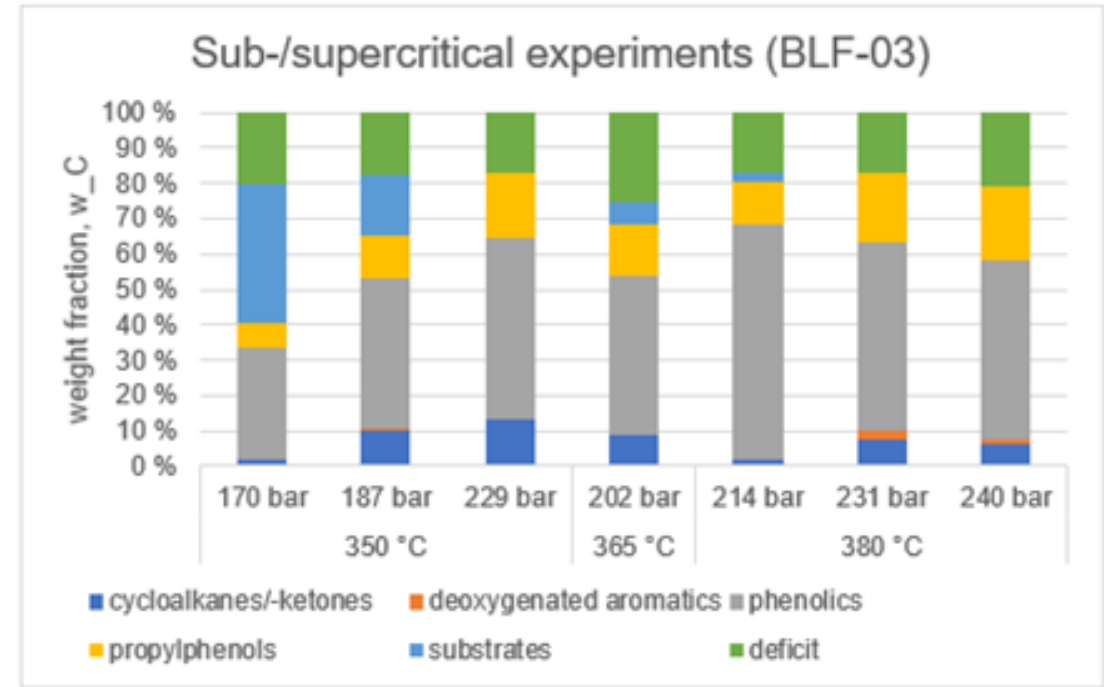
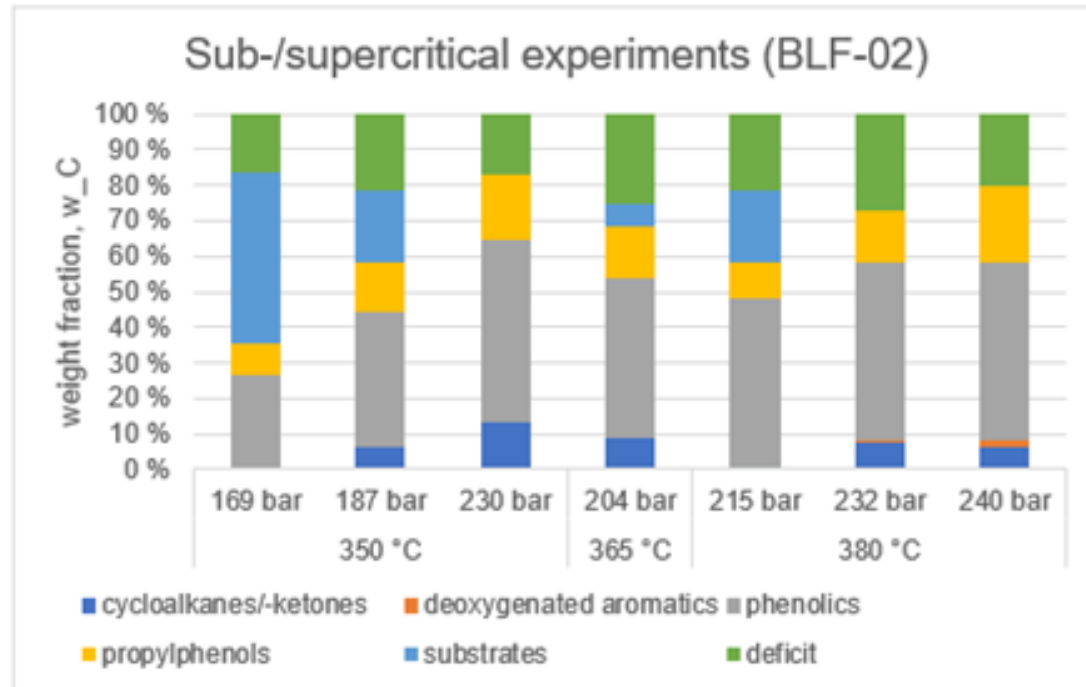
Green Chem., **23**, 2021, 1114; *Catalysis Communications*, **90**, 2017, 47-50; *Chemical Engineering Journal*, **407**, 2021, 126332.



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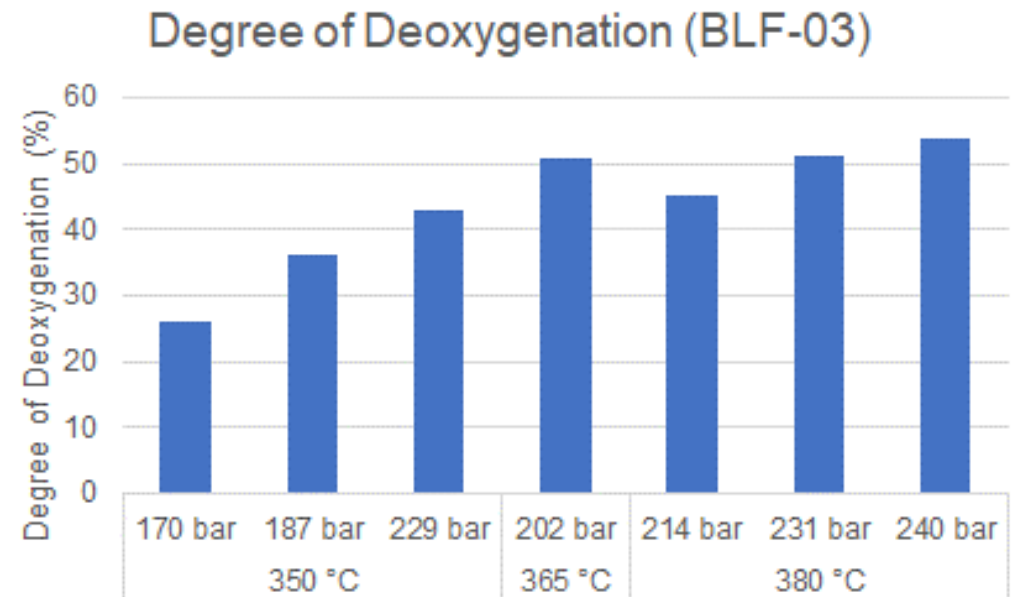
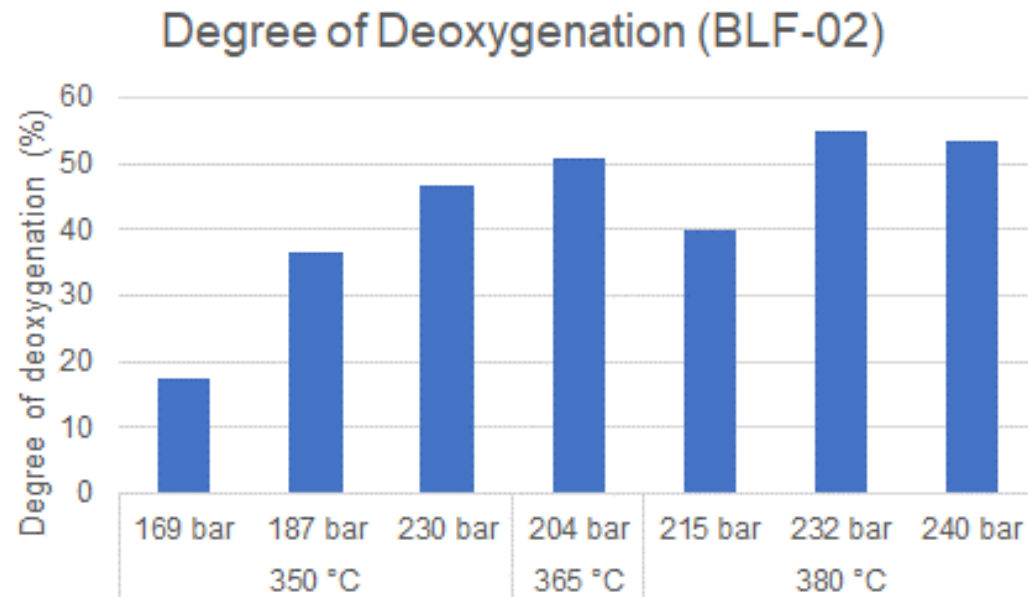
Hydrothermal HDO – model component testing

- HDO experiments of isoeugenol and 4-methylcatechol
 - 2 h reaction time, 2 g model compounds, 1g catalyst, 150 ml H₂O



Hydrothermal HDO – model component testing

- BLF-03 performs slightly better especially in the “milder” conditions



Summary

- Upgrading of bio-oils to transportation fuels challenging due to instability of bio-oils and impurities in bio-oils (sulfur etc.)
- New solutions needed to commercialize bio-oils upgrading by HDO
 - Slurry hydroprocessing (CaSH project)
 - Hydrothermal HDO (BL2F project)
- Catalysts have been developed and tested for these two upgrading technologies
 - So far mainly tests with model components
- Next steps: tests with real bio-oil feeds



Thank you!

Get in touch with the project:

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